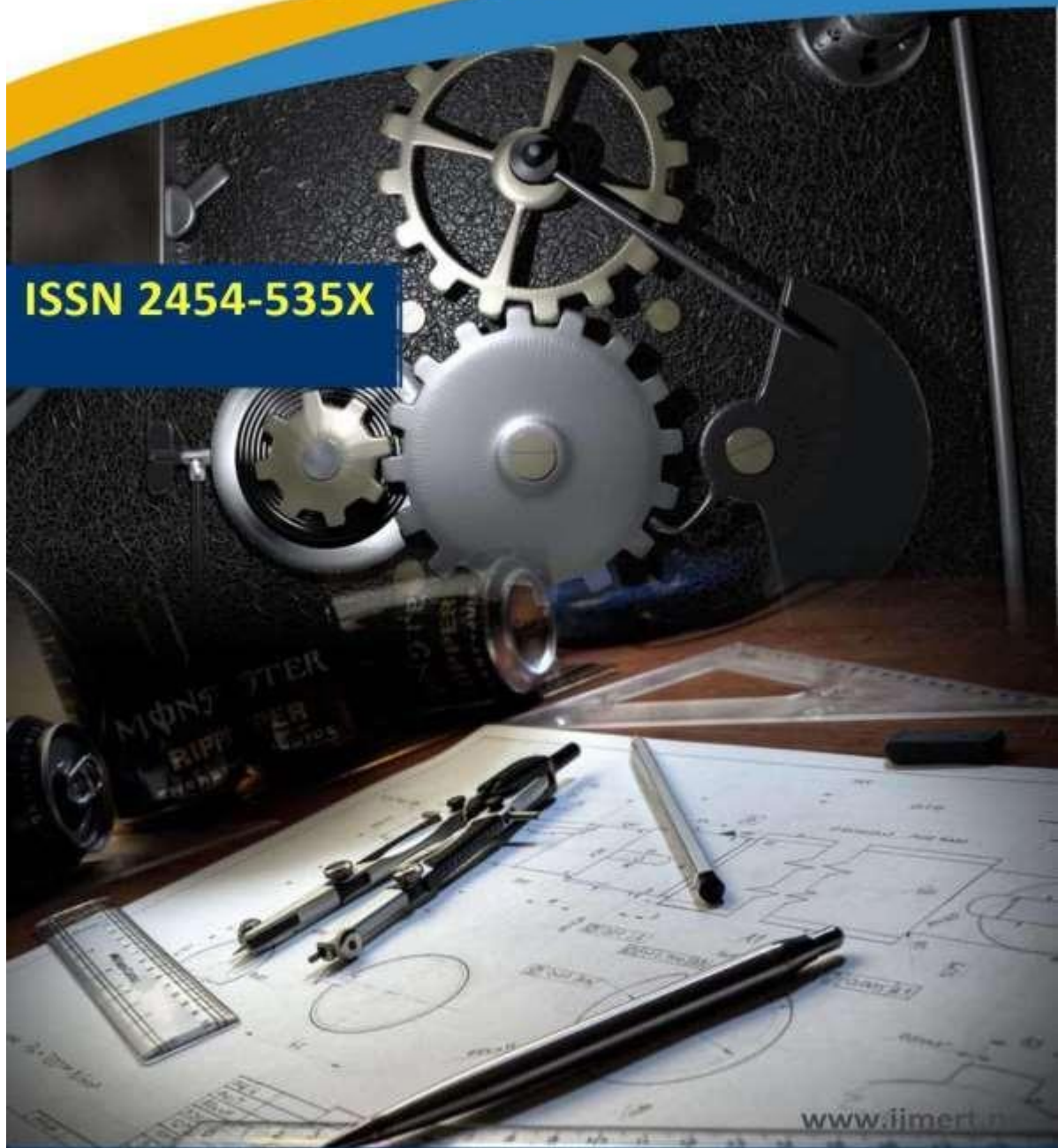




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A Kinetic Model for Predicting Temperature in Modified Atmosphere Packaging (MAP) for Hung Yen Longan

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ABSTRACT:

In a modified environment package (MAP), the fresh fruit's quality and shelf life must be preserved with careful temperature control inside the box. In this research, a kinetic model for MAP temperature prediction was built. The model was based on a system of differential equations that includes respiration heat (a Michaelis-Menten type equation), energy balances, and the phenomenon of gases flowing throughout the package. The fourth-order Runge-Kutta method was utilized to numerically solve the system equations. Using experiment data for different types of packing film, the model's usefulness for forecasting the temperature of MAP containing Hung Yen Longan was successfully verified

KEYWORDS: Longan; Respiration-Transpiration; Energy balances-gases transport phenomena;

INTRODUCTION

Eleven fruits, including Hung Yen Longan, have a significant potential for export from Vietnam. Unfortunately, there is still a significant loss of preservation time for both domestic and export demand as a result of the current technology's inability to store fresh longans after harvesting. One of the possible answers to this issue is the combination of low-temperature preservation technology and MAP, which has several benefits including a

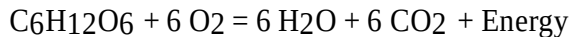
minimal chemical requirement for storage, cheap cost, and low energy usage.

Controlling the microclimate parameters of the environment surrounding fresh produce in the packaging, such as the gas concentration, the mixture gas's average temperature, the relative humidity, and any condensation that forms inside the package during storage, is what makes MAP technology so important. Within

MODEL DEVELOPMENT

Respiration model

The simple form of respiration equation is defined as following:



Applying to the respiratory case of fruits in MAP, then the respiration intensity can be considered as the reaction rate of the oxidation of glucose and other organic compounds in fruits. In which, O_2 is considered as a reactant, then according to the Michaelis-Menten model, we can determine the respiration rates as following:

$$R_{O_2} = \frac{V_{mO_2} \cdot O_2}{K_m + O_2} \quad (2)$$

For some fresh fruits, both O_2 and CO_2 concentrations have the effect of inhibiting respiratory reactions, affecting the quality and life time of fresh produce [2]. Chang et al. (1991) proposed three type of inhibition of enzyme reaction rates included competitive inhibition, uncompetitive inhibition, non-competitive inhibition. Based on the above three types of inhibition rates, have proposed the four types of inhibition in an enzyme kinetics models [2].

The type of "competitive inhibition" occurs when both the inhibitor and the reactant work together, when the CO_2 concentration is high, the concentration of O_2 increases strongly the intensity of O_2 absorption. The model of competitive influence is described as follows:

$$R_{O_2} = \frac{V_{mO_2} \cdot O_2}{K_m + O_2 + \frac{O_2 \cdot CO_2}{K_{ic}}} \quad (3)$$

Uncompetitive type occurs when CO_2 inhibitors do not react with enzymes, but react with enzyme-reactive compounds. In this case, increasing the concentration of O_2 at a high concentration of CO_2 hardly affects the consumption of O_2 . The model with non-competitive inhibition is described as follows:

$$R_{O_2} = \frac{V_{mO_2} \cdot O_2}{K_m + O_2 + \frac{O_2 \cdot CO_2}{K_{ic}}} \cdot \frac{1}{1 + \frac{CO_2}{K_{iu}}} \quad (4)$$

The "non-competitive" approach occurs when the reaction is inhibited both with enzymes and enzyme-substrate mixtures. This results, at high CO_2 concentrations, that the intensity of O_2 absorption will be in the range between the values obtained from the two inhibitory models described above. Non-competitive inhibition model is described in the following form:



$$R_2 = \frac{V_{O_2}}{mO_2} \left(\frac{K_1}{1 + \frac{CO_2}{K_2}} \right)$$

In the enzymatic reactions described above, only one enzyme is involved. However, in fact, the respiratory process has many enzymes that act together. This means that a "synthetic" form is needed to describe the change in gas concentration, which can combine both types of competition inhibition and non-competitive inhibition. This type of inhibition is called a combination inhibition and is described as follows:

$$R_2 = \frac{V_{O_2} \cdot mO_2}{K_1 + mO_2 + \frac{CO_2}{K_2} + \frac{mO_2 \cdot CO_2}{K_1 K_2}} \quad (6)$$

These four inhibition models will be tested for Hung Yen Longan. Then we evaluate the above models according to the level of applicable for Hung Yen Longan.

Temperature model The internal heat source, Q_{int} is the respiratory heat of produce and can be determined as follows: $Q_{int} = Q_S \cdot W_S$ (7)

Where, Q_S is the respiration heat and determined from equation (1). Assume that the respiratory intensity is the average of O_2 consumption and CO_2 evolution, then, Q_S is calculated as follows:

$$Q_S = \frac{2816}{6} \left(\frac{R_{O_2}}{2} + \frac{R_{CO_2}}{2} \right)$$

(8) Above equation is proposed by Kang và Lee. Factor α is considered as the convert factor from respiratory heat to energy and ranged from 0,8 to 1 (Burton, 1982; Powrie & Skura, 1991)

Factors RO_2 and RCO_2 is oxygen absorption intensity and carbonic emission intensity, respectively. RO_2 and RCO_2 can be calculated as follows [2-5].

The convection heat exchange between the produce surface and the gas inside the package is expressed as follows

$$Q_{ext} = h_s A_s (T_i - T_o)$$

The thermal equilibrium equation for fresh produce is built including the following thermal components: internal heat (respiratory heat), surface convection heat, latent heat of moisture escaping on the surface and current heat increases the fruit temperature [4]. The equation can be summarize as follows:

$$Q_{WhAT} = \frac{dT_s}{dt} \left(C_s m_s + \frac{m_1}{\lambda} \right) + Q_{ext} \quad (10)$$

where, m_1 is the evaporation rate from the fresh produce surface to the free gas layer in the package, λ is the vaporized latent heat and C_s is the specific heat capacity of produces. During the preservation, we can



consider T_i approximately equals T_s , then the equation (10) can be rewritten in a simple form as follows. These four inhibition models will be tested for Hung Yen Longan. Then we evaluate the above models according to the level of applicability for Hung Yen Longan. Temperature model The internal heat source, Q_{int} is the respiratory heat of produce and can be determined as follows: $Q_{int} = Q_S \cdot W_S$ (7) Where, Q_S is the respiration heat and determined from equation (1). Assume that the respiratory intensity is the average of O_2 consumption and CO_2 evolution, then, Q_S is calculated as follows:

$$Q_S = \frac{2816 \cdot R_O + R_{CO}}{6 \cdot 2} \quad (8)$$

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$$Q_{int} + Q_{ext} = W_s C_s \frac{dT_s}{dt} \quad (10)$$

where, m_1 is the evaporation rate from the fresh produce surface to the free gas layer in the package, λ is the vaporized latent heat and C_s is the specific heat capacity of produces.

During the preservation, we can consider T_i approximately equals T_s , then the equation (10) can be rewritten in a simple form as follows:

$$Q_{int} + Q_{ext} = W_s C_s \frac{dT_s}{dt} \quad (11)$$

The energy balance equation inside the package is defined as follows [4]:

$$Q_{int} + Q_{ext} = W_s C_s \frac{dT_s}{dt} + m_1 \lambda + \frac{dQ_{sp}}{dt} \quad (12)$$



For the initial conditions: $T_i = T_s$, i at $\tau = 0$, from equation (12), change the gas temperature in the package is determined as follows

$$\frac{dT_s}{dt} = \frac{h_p A (T_i - T_s)}{W_s C_s + W_a C_a} \quad (13)$$

here, h_p is the convective heat transfer coefficient of the packaging surface and is determined according to [4].

In summary, the temperature model consists of four nonlinear differential equations (2÷5), (16) and (13). This system is solved based on the 4th Runge-Kutta numerical method using Matlab software.

MATERIALS AND METHODS

Experimental subject The subject of experiment is Hung Yen Longan. The experiment was conducted with the untreated longan fruit with the time from harvest to experiment is within 24 hours. Experimental samples were tested at the second level of maturity. Fruit were treated before preservation included removing fruits

that are not properly ripened, crushed, scratched, rotten worms due to illness, birth; choosing fruit evenly for each experimental batch and cleaning mechanical impurities on the fruit surface. The fruit is stabilized in a cool place for a minimum of 12 hours and up to 24 hours before being tested. The sample of subject is shown in Figure 1.



Figure 1. Sample of Longan

Testing method

The method of measuring respiration rate is to measure the respiratory intensity of fresh produce in a closed system. The closed system method is performed by measuring O_2 and CO_2 concentrations over time in a closed container containing produce. This method is suitable for fruits and vegetables with low respiration rate and short experimental time.

The experiment was conducted in temperature

mode $4^\circ C$. The weight of each test sample is 1.0 kg putting in a plastic container with a sealed lid and the free volume of 5000 ml, as shown in Figure 2.

The testing procedure is taken in step by step included determining the weight of material sample W_s and determining the free volume V by overflowing method. The initial and final measurements are displayed directly on the 6600 Headspace Oxygen



/ carbon dioxide Analyzer (O₂, CO₂) screen. The material is measured for 96 hours with recording interval of 2 hours. **Figure 2.** Closed system

In order to ensure the reliability of the measurement results, the experiments were repeated 3 times and the results were analysed by the centralized method.

RESULTS AND DISCUSSIONS

Respiration model

Table 1 shows the parameters for respiration model at 4°C using Matlab. These values are used to identify respiration models according to 4

equations (2÷5), where the O₂ and CO₂ concentrations over time, produce weight, and free volume in closed systems were determined by experimental results.

Table 1. The repiration model parameters for T = 4°C

Model s		V _m	K _m	K _{mc}	K _{mu}	K _{mn}
1	O ₂	5.7439	3.5887	3.7896	-	-
	CO ₂	8.9482	2.3870	0.2613	-	-
2	O ₂	27.636 1	99.806 3	-	19.751 6	-
	CO ₂	8.4590	0.0001	-	2.1505	-
3	O ₂	6.5630	7.1096	-	-	27.259 7
	CO ₂	8.4588	0.0001	-	-	2.1507
4	O ₂	5.0387	0.3726	12.907 9	20.354 5	-
	CO ₂	8.6355	0.4549	80.782 7	2.1123	-

Validation of the respiration models Model 1: Competitive; Model 2: Uncompetitive;

Model 3: Noncompetitive; Model 4: Combination. The parameters of the respiration model in Table 1 were verified by comparing the predicted gas concentration from the respiration model and the experimental results of preserving the label in the closed system at a temperature of 4°C. The predicted gas concentration from the equation (2 ÷ 5), using the Runge-Kutta method, is simulated from the Fig.3 to Fig.6.

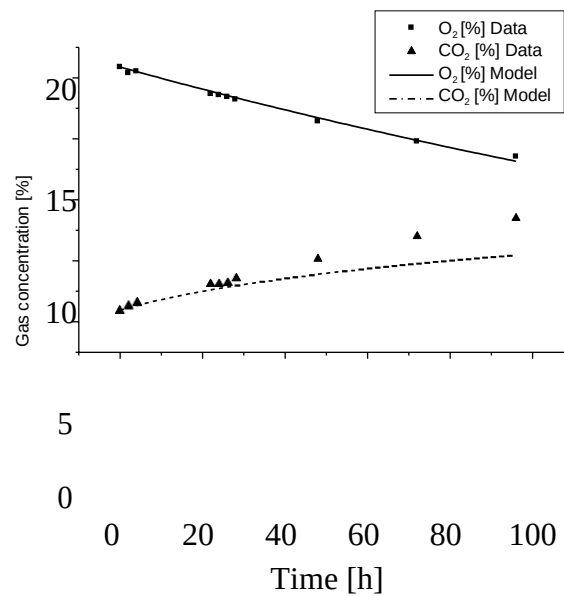
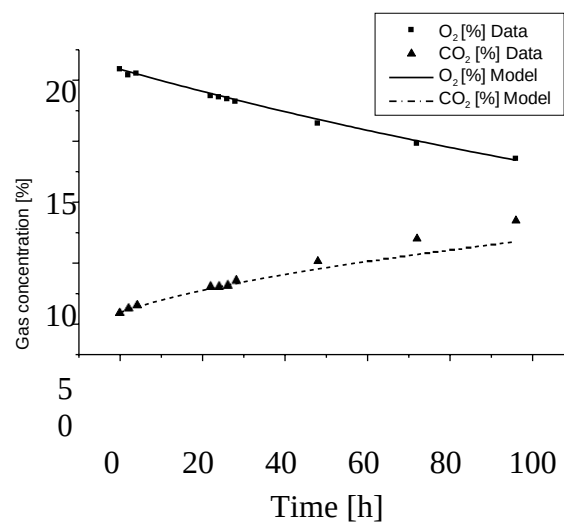
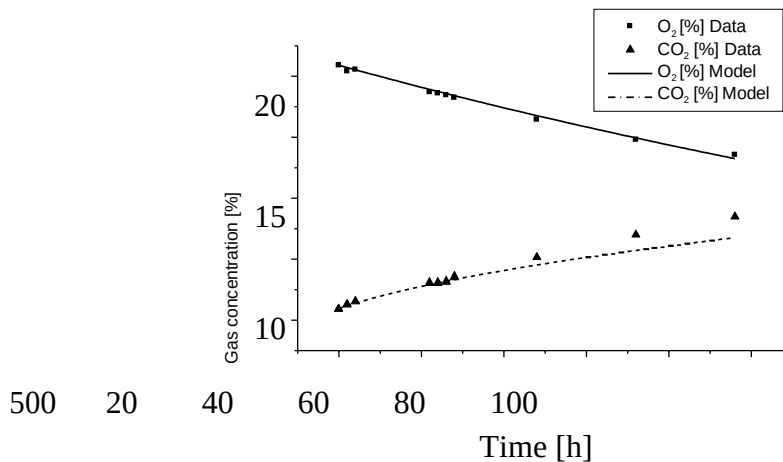
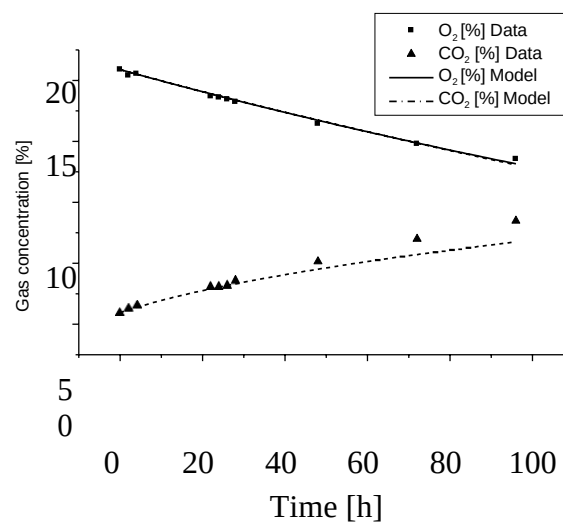


Figure 3. Validation of Competitive Model



**Figure 4.** Validation of Uncompetitive Model**Figure 5.** Validation of Noncompetitive Model**Figure 6.** Validation of combination Model The results from the

validation model show that:

- [O₂], [CO₂] determined from the models show the good agreement with $R^2_{O_2} > 0.99$ and $R^2_{CO_2} > 0.69$.
- The average relative errors for model 1 with [O₂] is 1.01%, [CO₂] is 17.25%. And square error $R^2_{O_2} = 0.9921$ and $R^2_{CO_2} = 0.6964$.
- The average relative errors for model 2 with [O₂] is 0.95%, [CO₂] is 8.50%. And square error $R^2_{O_2} = 0.9929$ and $R^2_{CO_2} = 0.9060$.

- The average relative errors for model 3 with [O₂] is 1.04%, [CO₂] is 8.50%. And square error $R^2_{O_2} = 0.9921$ and $R^2_{CO_2} = 0.9060$.
- The average relative errors for model 4 with [O₂] is 1.10%, [CO₂] is 8.50%. And square error $R^2_{O_2} = 0.9902$ and $R^2_{CO_2} = 0.9058$.
- Model 2 - uncompetitive show the best prediction with $R^2_{CO_2} = 0.9921$ and $R^2_{O_2} = 0.9060$; The average relative errors, respectively: [O₂] = 0.95%, [CO₂] = 8.5%, and the maximum relative errors for [O₂] is 2.10%, and for [CO₂] is 20.42%.

Validation of temperature model

Figure 7 illustrates the temperature field of the gas in the closed system. The results of the prediction model give the approximate results with experimental data. Thus, the application of respiration model for Hung Yen longan has been successfully verified in closed systems.

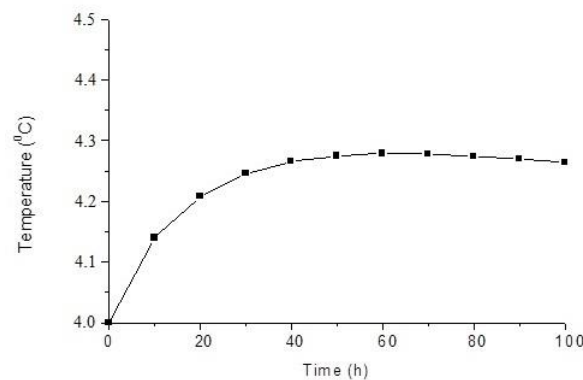


Figure 7. Temperature inside close system ($t_{mt} = 4^{\circ}\text{C}$)

CONCLUSIONS

In this paper, the respiration models for Hung Yen longan in MAP have been demonstrated. In four uncompetitive, in general, shows the best prediction with the $R^2 = 0.9921$ and $R^2 = 0.9060$, and the relative errors are smaller than

Michaelis-Menten models, the

CO₂



2.1% for O₂ and smaller than 20.42% for CO₂.
These are quite convincing results.

Moreover, respiration-evaporation model built on the basis of Michaelis-Menten formula combined with differential equations to express the energy equilibrium process shows the small errors. Based on that, the gas concentration prediction results, the temperature in the

packaging are highly accurate and can explain the actual process.

In summary, the proposed model in present study allows to shorten the time in designing of a suitable MAP package for the characteristics of each seasonal fruit, aiming to increase quality and extend the shelf life of fresh produce in actual production.

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